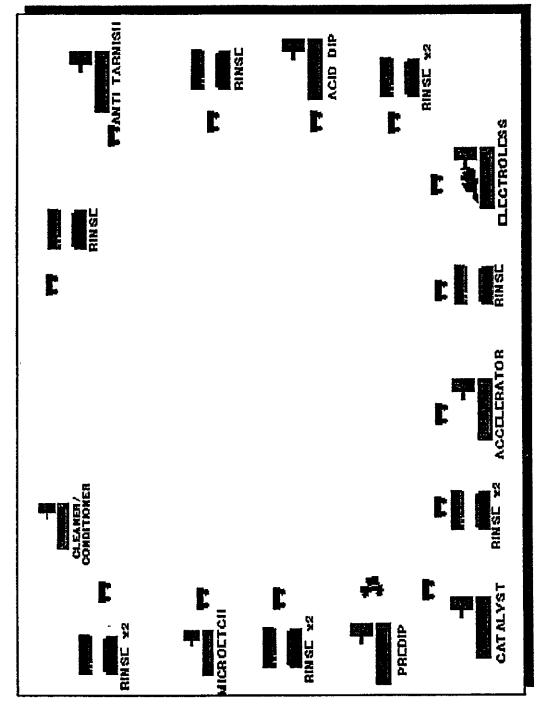
Appendix G

Supplemental Cost Analysis Information

- G.1 Graphic Representations of Cost Simulation Models for MHC Alternatives
- G.2 Bath Replacement Criteria for MHC Alternatives
- G.3 Bills of Activities for the MHC Process
- G.4 Simulation Model Outputs for MHC Alternatives
- G.5 Chemical Costs by Bath for Individual MHC Processes Total Materials Cost by MHC Alternative
- G.6 Sensitivity Analyses

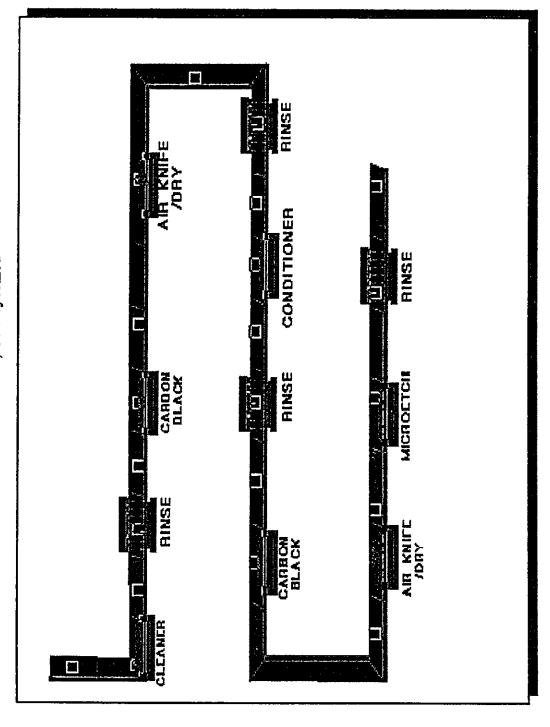
G.1	Graphic Representations of Cost Simulation Models for MHC Alternatives

Electroless Copper Process, Non-Conveyorized



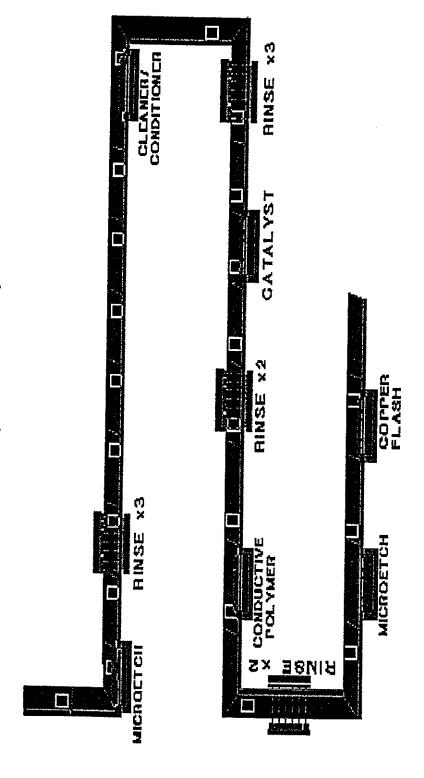
ANTI-TAGNIS RINSE HINSE x2 RINSE x2 RINSE HINSE x2 RINSE x2

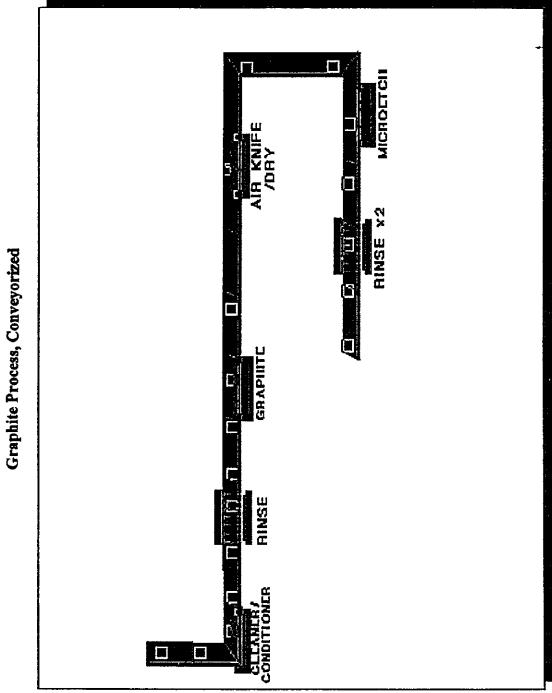
Electroless Copper Process, Conveyorized

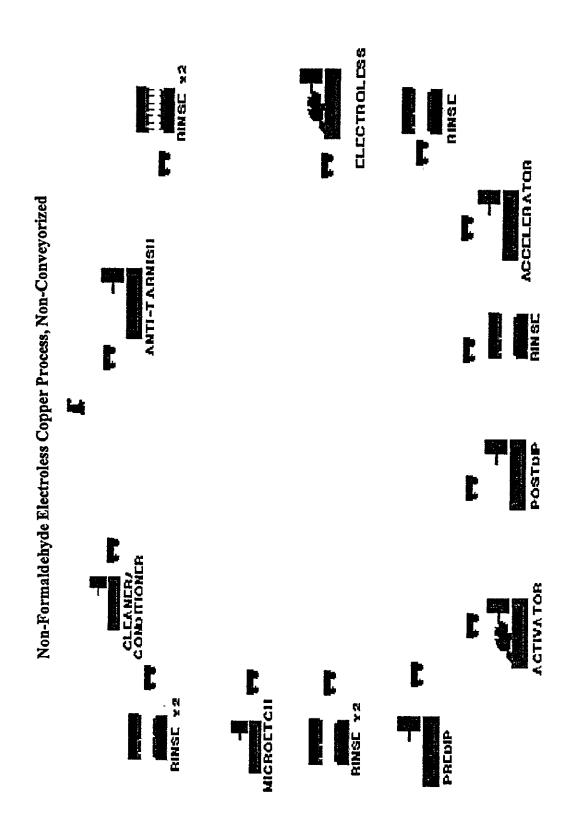


Carbon Process, Conveyorized

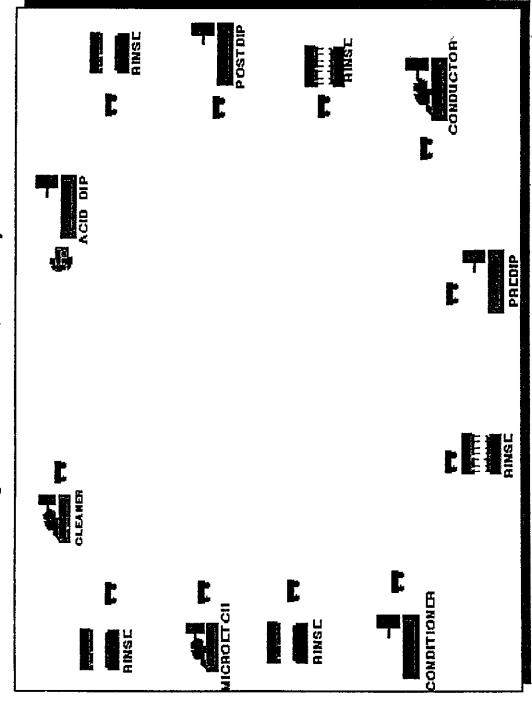
Conductive Polymer Process, Conveyorized







Organic-Palladium Process, Non-Conveyorized



HINSE PREDIP HINSE COMPUCTOR MICROETCII HINSE HINSE PINSE CLCANCR qiqtedq

Organic-Palladium Process, Conveyorized

ACCELERA IOR RINSE x2 RINSE Y2 GA IALYSI AGID DIP Tin-Palladium Process, Non-Conveyorized PREDIP HINSE x2 KINSE YZ

PALL ADIUM CATALYST HINSE x2 ACCOLERATOR HINSE x2 dioA 410

Tin-Palladium Process, Conveyorized

G.2	Bath Replacement Criteria for MHC Alternatives

Electroless Copper - Non-Conveyorized (Baseline) Electroless Copper - Conveyorized

Non-Formaldehyde Electroless Copper - Non-Conveyorized^A

		Bath Re	placeme	Frequency of Replacement Cost Simulation Inputs ³				
Process Step	Process # 1	Process # 2	Process # 3	Process # 4	Process # 5	O	Conveyorized (Panels)	Non- Conveyorized (Racks)
Cleaner/Conditioner	Conc.	228	500	300	1,000	510	5,920	396
Micro-Etch	Conc.	ND	250	ND	Conc.	250	2,858	194
Predip	Conc.	228	Conc.	400	1,000	540	4,822	418
Catalyst	300	Conc.	500	6 mos	Conc.	1/year	1/year	1/year
Post Dip/Acid Dip	ND	ND	1,000	ND	350	675	9,523	523
Accelerator	360	160	2,500 *	250	350	280	4,000	217
Electroless Copper	360	Conc.	500	ND	Conc.	430	14,206	334
Anti-Tarnish	200	ND	250	ND	500	325	2,264	252

ND = No Data

NA = Not Applicable

Conc. = Replacement data given in concentration (e.g, g/L Cu) so not usable in this analysis.

To calculate racks per bath replacement, multiply average frequency of replacement by 75 gallons (average bath size) and divide by 96.8 ssf/rack.

^{* -} data point considered outlier and thus not included in calculation of average.

^A Incomplete bath replacement data submitted for non-formaldehyde copper process. Therefore, the process was assumed to be similar to electroless copper for the purposes of bath replacement.

¹ Bath replacement frequency data for MHC product lines reported on product data sheets provided by chemical supplier of each individual process.

² Reported value was calculated by excluding any outlying values and then averaging remaining bath replacement data for each bath.

³ To calculate panels per bath replacement, multiply average frequency of replacement by bath size in gallons and divide by 5.6 ssf/panel.

Carbon - Conveyorized

		Bath Ro	eplaceme	Frequency of Replacement Cost Simulation Inputs ³				
Process Step	Process # 1	Process # 2	Process # 3	Process # 4	Process # 5	Average Frequency of Replacement ²	Conveyorized (Panels)	Non- Conveyorized (Racks)
Cleaner	300	NA	NA	NA	NA	300	2,340	NA
Carbon Black	1/year	NA	NA	NA	NA	1/year	1/year	NA
Conditioner	300	NA	NA	NA	NA	300	2,961	NA
Carbon Black	1/year	NA	NA	NA	NA	1/year	1/year	NA
Micro-Etch	ND	NA	NA	NA	NA	250**	2,855	NA

NA = No Data

NA = Not Applicable

Conc. = Replacement data given in concentration (e.g., g/L Cu) so not usable in this analysis.

^{** -} Due to lack of replacement data, the frequency of replacement of the micro-etch bath was assumed to the same as for electroless copper.

¹ Bath replacement frequency data for MHC product lines reported on product data sheets provided by chemical supplier of each individual process.

² Reported value was calculated by excluding any outlying values and then averaging remaining bath replacement data for each bath.

³ To calculate panels per bath replacement, multiply average frequency of replacement by bath size in gallons and divide by 5.6 ssf/panel.

Conductive Polymer - Conveyorized

		Bath Re	placeme	Frequency of Replacement Cost Simulation Inputs ³				
Process Step	Process # 1	Process # 2	Process # 3	Process # 4	Process # 5	0	Conveyorized (Panels)	Non- Conveyorized (Racks)
Micro-Etch	ND	NA	NA	NA	NA	250**	2,855	NA
Cleaner/Conditioner	408	NA	NA	NA	NA	410	4,681	NA
Cleaner/Conditioner	408	NA	NA	NA	NA	410	4,681	NA
Catalyst	4,880	NA	NA	NA	NA	4,880	11,985	NA
Conductive Polymer	1,935	NA	NA	NA	NA	1,940	8,918	NA
Micro-Etch	ND	NA	NA	NA	NA	250**	2,855	NA

NA = No Data

NA = Not Applicable

Conc. = Replacement data given in concentration (e.g., g/L Cu) so not usable in this analysis.

^{** -} Due to lack of replacement data, the frequency of replacement of the micro-etch bath was assumed to the same as for electroless copper.

¹ Bath replacement frequency data for MHC product lines reported on product data sheets provided by chemical supplier of each individual process.

² Reported value was calculated by excluding any outlying values and then averaging remaining bath replacement data for each bath.

³ To calculate panels per bath replacement, multiply average frequency of replacement by bath size in gallons and divide by 5.6 ssf/panel.

Organic Palladium - Conveyorized Organic Palladium - Non-Conveyorized

		Bath Ro	eplacemo	Frequency of Replacement Cost Simulation Inputs ³				
Process Step	Process # 1	Process # 2	Process # 3	Process # 4	Process # 5	0	Conveyorized (Panels)	Non- Conveyorized (Racks)
Cleaner	200	NA	NA	NA	NA	200	1,560	155
Micro-Etch	ND	NA	NA	NA	NA	250**	2,855	194
Conditioner	244	NA	NA	NA	NA	240	2,411	189
Predip	1/week	NA	NA	NA	NA	1/week	1/week	NA
Conductor	2,038	NA	NA	NA	NA	2,040	39,007	1,580
Post Dip	244	NA	NA	NA	NA	240	1,950	189
Acid Dip	200	NA	NA	NA	NA	200	2,801	155

ND = No Data

NA = Not Applicable

Conc. = Replacement data given in concentration (e.g, g/L Cu) so not usable in this analysis.

To calculate racks per bath replacement, multiply average frequency of replacement by 75 gallons (average bath size) and divide by 96.8 ssf/rack.

^{** -} Due to lack of replacement data, the frequency of replacement of the micro-etch bath was assumed to be the same as for electroless copper.

¹ Bath replacement frequency data for MHC product lines reported on product data sheets provided by chemical supplier of each individual process.

² Reported value was calculated by excluding any outlying values and then averaging remaining bath replacement data for each bath.

³ To calculate panels per bath replacement, multiply average frequency of replacement by bath size in gallons and divide by 5.6 ssf/panel.

Graphite - Conveyorized

		Bath Re	placeme	Frequency of Replacement Cost Simulation Inputs ³				
Process Step	Process # 1	Process # 2	Process # 3	Process # 4	Process # 5	0	Conveyorized (Panels)	Non- Conveyorized (Racks)
Cleaner/Conditioner	200	750	NA	NA	NA	475	5,443	NA
Graphite	Conc.	3,000	NA	NA	NA	3,000	19,415	NA
Micro-Etch	Conc.	ND	NA	NA	NA	250**	2,855	NA

ND = No Data

NA = Not Applicable

Conc. = Replacement data given in concentration (e.g, g/L Cu) so not usable in this analysis.

^{** -} Due to lack of replacement data, the frequency of replacement of the micro-etch bath was assumed to be the same as for electroless copper.

¹ Bath replacement frequency data for MHC product lines reported on product data sheets provided by chemical supplier of each individual process.

² Reported value was calculated by excluding any outlying values and then averaging remaining bath replacement data for each bath.

³ To calculate panels per bath replacement, multiply average frequency of replacement by bath size in gallons and divide by 5.6 ssf/panel.

Tin-Palladium - Conveyorized Tin-Palladium - Non-Conveyorized

		Bath Re	placeme	Frequency of Replacement Cost Simulation Inputs ³				
Process Step	Process # 1	Process # 2	Process # 3	Process # 4	Process # 5	0	Conveyorized (Panels)	Non- Conveyorized (Racks)
Cleaner/Conditioner	350	1,000	500	2 weeks	NA	610	6,879	465
Micro-Etch	Conc.	Conc.	250	Conc.	NA	250**	2,855	194
Predip	400	4,000*	500	Conc.	NA	450	3,972	349
Catalyst	3,000	Conc.	2,500	1,000	NA	1/year	1/year	1/year
Accelerator	500	1,000	500	400	NA	600	8,457	465
Acid Dip	500	ND	1,000	210	NA	570	7,961	442

ND = No Data

NA = Not Applicable

Conc. = Replacement data given in concentration (e.g, g/L Cu) so not usable in this analysis.

- ** Due to lack of replacement data, the frequency of replacement of the micro-etch bath was assumed to be the same as for electroless copper.
- ¹ Bath replacement frequency data for MHC product lines reported on product data sheets provided by chemical supplier of each individual process.
- ² Reported value was calculated by excluding any outlying values and then averaging remaining bath replacement data for each bath.
- ³ To calculate panels per bath replacement, multiply average frequency of replacement by bath size in gallons and divide by 5.6 ssf/panel.

To calculate racks per bath replacement, multiply average frequency of replacement by 75 gallons (average bath size) and divide by 96.8 ssf/rack.

APPENDIX	G
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G.3	Bills of Activities for the MHC Process

Activities Associated with the Bath Setup

Activity Description		Cost Driver	Cost/Activity
Wear masks, goggles, rubber gloves, and suitable of	clothing	\$/bath setup	\$2.50
Go to storage area		labor	
Locate protective equipment		labor	
Put on protective equipment		labor	
		protective equipment	
Return to tank		labor	
Put in base liquid (usually water)		\$/bath setup	\$2.60
Open water valve		labor	
Wait for measured amount		labor	
Close water valve		labor	
Document water amount/level		labor	
Mix the bath solution		\$/bath setup	\$5.00
Open the chemical containers		labor	
Add the chemicals to the bath		labor	
Turn on the agitator		labor	
Wait for mixing		labor	
Turn off the agitator		labor	
Titrate sample		labor	
Document		labor	
Repeat as necessary		labor	
Flush containers		\$/bath setup	\$3.00
Turn on water valve		labor	
Spray containers		labor	
Turn off water valve		labor	
Place empty container in storage area		\$/bath setup	\$2.00
Take container to storage		labor	
Documentation		labor	
Return to tank		labor	
	Total =	\$per testing	\$15.10

Activities Associated with the Tank Cleanup

Activity Description	Cost Driver	Cost/Activity
Rinse with water	\$/cleanup	\$25.00
Obtain spray/rinse equipment	labor	
Turn water on	labor	
Spray equipment	labor	
Turn water off	labor	
Obtain scrubbing and cleaning tools	\$/cleanup	\$1.00
Go to storage area	labor	
Find necessary tools	labor	
Return to tank	labor	
Hand scrub tank	\$/cleanup	\$30.00
Put on gloves, choose tool	labor	
Scrub tank	labor	
	cleaning supplies	
Return cleaning tools	\$/cleanup	\$1.25
Go to the storage area	labor	
Place tools in correct place	labor	
Return to tank	labor	
Spray according to schedule	\$/cleanup	\$5.00
Wait for time to elapse before spraying	labor	
Obtain spray equipment	labor	
Turn spray on	labor	
Spray all cleaning solution from tank	labor	
Turn spray off	labor	
Operator opens control valve	\$/cleanup	\$1.00
Find correct control valve	labor	
Open valve	labor	
Water goes to treatment facility	\$/cleanup	\$2.75
Wait for water to drain	labor	
Operator closes control valve	\$/cleanup	\$1.00
Locate correct control valve	labor	
Close valve	labor	
Т	otal = \$per testing	\$67.00

Activities Associated with Sampling and Testing

Activity Description	Cost Driver	Cost/Activity
Get sample	\$/testing	\$1.35
Go to the line	labor	
Titrate small sample into flask	labor	
	materials	
Transfer to lab	labor	
Test sample	\$/testing	\$1.35
Request testing chemicals	labor	
Document request	labor	
Locate chemicals	labor	
Add chemicals to sample	labor	
	materials	
Mix	labor	
Document the results	labor	
Return testing chemicals	labor	
Relay information to line operator	\$/testing	\$1.00
Return to line	labor	
Inform operator of results	labor	
Document	labor	
Tota	l = \$per testing	\$3.70

Activities Associated with Filter Replacement

Activity Description	Cost Driver	Cost/Activity
Check old filter	\$/replacement	\$1.50
Pull canister from process	labor	
Inspect filter	labor	
Decide if replacement is necessary	labor	
Get new filer	\$/replacement	\$1.75
Go to storage area	labor	
Locate new filters	labor	
Fill out paper work	labor	
Return to tank	labor	
Change filter	\$/replacement	\$12.25
Pull old filter from canister	labor	
Replace with new filter	labor	
	filter	
Replace canister	labor	
Fill out paper work	labor	
Dispose of old filter	\$/replacement	\$2.00
Take old filter to disposal bin/area	labor	
Dispose of filter	labor	
Return to tank	labor	
Fill out paper work	labor	
	Total = \$per replacement	\$17.50

G.4	Simulation Model Outputs for MHC Alternatives

Summary for Replication 1 of 1

Project: VERTICAL GENERIC ELECTRO

Run execution date : 6/10/1997 Analyst: CHAD TONEY Model revision date: 7/10/1996

Replication ended at time

: 163453.0

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations		
TAKT TIME	45.201	.81575	34.000	306.00	3615		
TIME IN SYSTEM	49.271	9.8667E-04	49.116	49.333	3616		
TIME STOPPED	80.408	.69205	.00000	271.97	422		
DISCRETE-CHANGE VARIABLES							
Identifier	Average	Variation	Minimum	Maximum	Final Value		
CARRIER Active	15.000	.00000	15.000	15.000	15.000		
CARRIER Busy	.01106	9.4553	.00000	1.0000	.00000		
# in ACCELERATOR Q	.00148	26.015	.00000	1.0000	.00000		
# in ACID DIP_Q	.00147	26.019	.00000	1.0000	.00000		
# in CATALYST_Q	.00148	26.015	.00000	1.0000	.00000		
# in CLEAN Q	8.3941E-04	34.500	.00000	1.0000	.00000		
# in ELECTROLESS Q	.00192	22.819	.00000	1.0000	.00000		
# in MICROETCH Q	.00148	26.015	.00000	1.0000	.00000		
# in PREDIP_Q	.00148	26.015	.00000	1.0000	.00000		
# in RINSE1 Q	.00148	26.015	.00000	1.0000	.00000		
# in RINSE2_Q	.00148	26.015	.00000	1.0000	.00000		
# in RINSE3_Q	.00148	26.015	.00000	1.0000	.00000		
# in RINSE4 Q	.00148	25.999	.00000	1.0000	.00000		
# in RINSE5 Q	.00147	26.019	.00000	1.0000	.00000		
# in RINSE6 Q	.00147	26.019	.00000	1.0000	.00000		
# in RINSE7 Q	.00147	26.019	.00000	1.0000	.00000		
# in STARTING Q	.00000		.00000	.00000	.00000		
# in TARNISH Q	.00147	26.019	.00000	1.0000	.00000		
# in CLEAN1 Q	.00000		.00000	.00000	.00000		
# in MICROETCH1 Q	.00000		.00000	.00000	.00000		
# in PREDIP1 Q	.00000		.00000	.00000	.00000		
# in CATALYST1 Q	.00000		.00000	.00000	.00000		
# in ACCELERATOR1 Q	.00000		.00000	.00000	.00000		
# in ELECTROLESS1 Q	.00000		.00000	.00000	.00000		
# in ACID DIP1 Q	.00000		.00000	.00000	.00000		
# in TARNISH1_Q	.00000	~-	.00000	.00000	.00000		

COUNTERS

Identifier	Count	Limit
PARTS DONE	3616	Infinite

FREQUENCIES

Identifier	Category	Occur Number	rences AvgTime	Standard Percent	Restricted Percent
STATE (CLEAN1 R)	CLEAN BATH	9	138.22	0.76	0.76
_	BUSY	400	92.965	22.75	22.75
	IDLE	403	310.23	76.49	76.49
STATE (MICROETCH1 R)	MICRO BATH	18	145.66	1.60	1.60
_	BUSY	400	94.395	23.10	23.10
	IDLE	405	303.88	75.30	75.30
STATE (PREDIP1_R)	PREDIP BATH	8	124.50	0.61	0.61
- '	BUSY	400	95.790	23.44	23.44
	IDLE	402	308.80	75.95	75.95
STATE (CATALYST1_R)	CATAL BATH	1	230.00	0.14	0.14
_	BUSY	400	95.485	23.37	23.37
	IDLE	401	311.79	76.49	76.49
STATE (ACCELERATOR1_R)	ACCEL BATH	16	129.75	1.27	1.27
_	BUSY	400	97.560	23.87	23.87
	IDLE	405	302.10	74.86	74.86
STATE (ELECTROLESS1_R)	ELECT BATH	10	113.60	0.70	0.70
-	BUSY	400	98.875	24.20	24.20
	IDLE	401	306.15	75.11	75.11
STATE (ACID DIP1 R)	ACID BATH	6	146.00	0.54	0.54
	BUSY	400	99.445	24.34	24.34
	IDLE	401	306.23	75.13	75.13
STATE (TARNISH1 R)	TARN BATH	13	119.53	0.95	0.95
***- ·	BUSY	400	101.42	24.82	24.82
	IDLE	404	300.31	74.23	74.23

Execution time: 75.62 minutes. Simulation run complete.

Summary for Replication 1 of 1

Project: TYPICAL CARBON CONVEYORIZED Analyst: CHAD TONEY

Run execution date: 10/4/1996 Model revision date: 7/11/1996

Replication ended at time

50808.6

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME TIME IN SYSTEM	.81854 47.610	6.7748 1.0902	.60608 12.996	195.00 257.69	62056 62057
TIME STOPPED	74.507	1.0634	14.000	208.92	158
	DISCR	ETE-CHANGE V	ARIABLES		
Identifier	Averaĝe	Variation	Minimum	Maximum	Final Value
# in TO_CLEANER_Q	.00145	26.200	.00000	1.0000	.00000
		COUNTERS			
	Identifier		Count	Limit	
	<u> </u>			<u> </u>	

parts done

62057 Infinite

FREQUENCIES

Identifier	Category	Occur Number	rences AvgTime	Standard Percent	Restricted Percent
STATE (CLEAN_R)	CLEAN BATH	26	147.01	7.52	7.52
	BUSY	124	12.460	3.04	3.04
	IDLE	136	334.12	89.44	89.44
STATE (MICROETCH_R)	MICRO BATH	21	160.66	6.64	6.64
	BUSY	124	24.645	6.01	6.01
	IDLE	138	321.58	87.34	87.34
STATE (CARBON_R)	BUSY	124	12.460	3.04	3.04
	IDLE	125	394.10	96.96	96.96
STATE (CONDITIONER_R)	CONDI BATH	20	142.03	5.59	5.59
	BUSY	124	19.674	4.80	4.80
	IDLE	134	339.76	89.61	89.61
STATE (CARBON2_R)	BUSY	124	19.674	4.80	4.80
	IDLE	125	386.95	95.20	95.20

Execution time: 32.93 minutes.

Summary for Replication 1 of 1

Project: CONVEYORIZED TYPICAL CON Analyst: CHAD TONEY

Run execution date : Model revision date:

6/11/1997 7/10/1996

Replication ended at time

: 29091.1

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME	.46866	9.1628	.35294	190.00	62056
TIME IN SYSTEM TIME STOPPED	38.993 77.321	1.2748 .99426	8.0000 .0000	216.01 192.20	62057 92
	DISCR	ETE-CHANGE V	ARIABLES		
Identifier	Average	Variation	Minimum	Maximum	Final Value
# in TO_MICROETCHER_Q	.36856	1.3089	.00000	1.0000	1.0000
		COUNTERS			
Id	lentifi e r		Count	Limit	
P.F	RTS DONE		62057 1	nfinite	

FREQUENCIES

Identifier	Category		rences AvgTime	Standard Percent	Restricted Percent
STATE (CLEAN R)	CLEAN BATH	13	150.96	6.75	6.75
-	BUSY	71	21.147	5.16	5.16
	IDLE	78	328.55	88.09	88.09
STATE (MICROETCH R)	MICRO BATH	21	145.76	10.52	10.52
	BUSY	71	15.567	3.80	3.80
	IDLE	82	303.96	85.68	85.68
STATE (CATALYST R)	BUSY	71	21.147	5.16	5.16
· · · · · · · · · · · · · · · · · · ·	IDLE	72	383.18	94.84	94.84
STATE (CONDUCT R)	CONDUCT BATH	6	135.43	2.79	2.79
	BUSY	71	24.971	6.09	
	IDLE	75	353.40	91.11	91.11
STATE (MICROETCH2 R)	MICRO2 BATH	21	145.76	10.52	10.52
	BUSY	71	24.971	6.09	6.09
	IDLE	82	295.81	83.38	83.38
STATE (CLEAN2 R)	CLEAN2 BATH	13	150.96	6.75	6.75
	BUSY	71	21.147	5.16	5.16
	IDLE	78	328.55	88.09	88.09

Execution time: 25.02 minutes. Simulation run complete.

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Summary for Replication 1 of 1

Project: CONVEYORIZED GENERIC ELE Analyst: CHAD TONEY

Run execution date : 6/10/1997 Model revision date: 7/ 9/1996

Replication ended at time

TALLY VARIABLES

: 36063.0

Ídentifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME	.58089	11.492	.31433	195.00	62056
TIME IN SYSTEM TIME STOPPED	52.938 114.06	1.1157 .69924	14.998 .00000	282.95 211.27	62057 143
	DISCR	ETE-CHANGE V	ARIABLES		
Identifier	Average	Variation	Minimum	Maximum	Final Value
# in TO_CLEANER_Q	.00259	19.641	.00000	1.0000	.00000
		COUNTERS			
	Identifier		Count	Limit	
	PARTS DONE		62057	Infinite	

FREQUENCIES

Identifier	Category		rences AvgTime	Standard Percent	Restricted Percent
STATE (ACCELERATOR_R)	ACCEL BATH	15	160.23	6.66	6.66
	BUSY IDLE	88 95	29.890 326.62	7.29 86.04	7.29 86.04
STATE (CLEAN R)	CLEAN BATH	10	168.71	4.68	4.68
_ ,	BUSY IDLE	88 96	11.362 347.66	2.77 92.55	2.77 92.55
STATE (ELECTROLESS R)	ELECT BATH	4	135.81	1.51	1.51
_	BUSY IDLE	88 91	32.154 359.23	7.85 90.65	7.85 90.65
STATE (ACID DIP_R)	ACID BATH	6	174.40	2.90	2.90
_	BUSY IDLE	88 91	33.135 352.75	8. 0 9 89.01	8.09 89.01
STATE (MICROETCH_R)	MICRO BATH	21	165.74	9.65	9.65
	BUSY IDLE	88 102	16.644 305.07	4.06 86.29	4.06 86.29

STATE (CATALYST_R)	BUSY	88	25.024	6.11	6.11
	IDLE	89	380.45	93.89	93. 8 9
STATE (PREDIP_R)	PREDIP BATH	13	126.76	4.57	4.57
	BUSY	88	25.024	6.11	6.11
	IDLE	93	346.37	89.32	89.32
STATE (TARNISH_R)	TARN BATH	28	146.91	11.41	11.41
	BUSY	88	45.458	11.09	11.09
	IDLE	100	279.48	77.50	77.50

Execution time: 35.08 minutes. Simulation run complete.

SIMAN V - License #9999999 Systems Modeling Corporation

Summary for Replication 1 of 1

Project: GRAPHITE CONVEYORIZED Analyst: CHAD TONEY

Run execution date : 10/7/1996 Model revision date: 7/11/1996

62057 Infinite

Replication ended at time

: 33441.3

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME	.53876	8.2863	.43032	230.00	62056
TIME IN SYSTEM	50.811	1.3392	7.7983	262.99	62057
TIME STOPPED	66.957	1.3307	10.000	230.00	97
	DISCR	ETE-CHANGE V	ARIABLES		
Identifier	Average	Variation	Minimum	Maximum	Final Value
KNIFE R Available	1.0000	.00000	1.0000	1.0000	1.0000
KNIFE R Busy	.00000		.00000	1.0000	.00000
# in TO_CLEANER_Q	.05939	3.9795	.00000	1.0000	-00000
		COUNTERS			
	Identifier		Count	Limit	

FREQUENCIES

PARTS DONE

Identifier	Category	Occur Number	rences AvgTime	Standard Percent	Restricted Percent	
STATE (CLEAN_R)	CLEAN BATH	11	146.08	4.81	4.81	
	BUSY	81	13.067	3.17	3.17	
	IDLE	85	362.06	92.03	92.03	
STATE (MICROETCH_R)	MICRO BATH	21	169.72	10.66	10.66	
-	BUSY	81	29.377	7.12	7.12	
	IDLE	93	295.67	82.23	82.23	
STATE (GRAPHITE R)	GRAPH BATH	3	171.19	1.54	1.54	
· — ·	BUSY	81	14.975	3.63	3.63	
	IDLE	83	382.10	94.84	94.84	

Execution time: 19.63 minutes. Simulation run complete.

Summary, for Replication 1 of 1

Project: VERTICAL NONFORMALDEHYDE Analyst: CHAD TONEY

Run execution date: 7/ 1/1997 Model revision date: 5/13/1996

Replication ended at time

TALLY VARIABLES

: 73313.7

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME TIME IN SYSTEM TIME STOPPED	20.266 49.864 62.084	.81589 .04022 .24716	15.900 49.600 .00000	160.00 66.400 127.82	3615 3616 243
	DISCRI	ete-change v	ARIABLES		
Identifier	Average	Variation	Minimum	Maximum	Final Value
ACCELERATOR_R Availabl	1.0000	.00000	1.0000	1.0000	1.0000
ACCELERATOR R Busy	.12334	2.6660	.00000	1.0000	.00000
CLEAN_R Available	1.0000	.00000	1.0000	1.0000	1.0000
CLEAN_R Busy	.12340	2.6653	.00000	1.0000	1.0000
ACTIVATOR_R Available	1.0000	.00000	1.0000	1.0000	1.0000
ACTIVATOR R Busy	.12337	2.6656	.00000	1.0000	.00000
ELECTROLESS_R Availabl	1.0000	.00000	1.0000	1.0000	1.0000
ELECTROLESS R Busy	.77594	.53736	.00000	1.0000	1.0000
FLASH_R Available	1.0000	.00000	1.0000	1.0000	1.0000
FLASH_R Busy	.12331	2.6664	.00000	1.0000	.00000
MICROETCH_R Available	1.0000	.00000	1.0000	1.0000	1.0000
MICROETCH_R Busy	.12337	2.6656	.00000	1.0000	.00000
POSTDIP_R Available	1.0000	.00000	1.0000	1.0000	1.0000
POSTDIP_R Busy	.12337	2.6656	.00000	1.0000	1.0000
PREDIP_R Available	1.0000	.00000	1.0000	1.0000	1.0000
PREDIP_R Busy	.12337	2.6656	.00000	1.0000	.00000
RINSE1_R Available	1.0000	.00000	1.0000	1.0000	1.0000
RINSE1_R Busy	.12337	2.6656	.00000	1.0000	.00000
RINSE2_R Available	1.0000	.00000	1.0000	1.0000	1.0000
RINSE2_R Busy	.12337	2.665 6	.00000	1.0000	.00000
RINSE3_R Available	1.0000	.00000	1.0000	1.0000	1.0000
RINSE3_R Busy	.12334	2.6660	.00000	1.0000	.00000
RINSE4_R Available	1.0000	.00000	1.0000	1.0000	1.0000
RINSE4 R Busy	.12334	2.6660	.00000	1.0000	.00000
TARNISH_R Available	1.0000	.00000	1.0000	1.0000	1.0000
TARNISH_R Busy	.12331	2.6664	.00000	1.0000	.00000
RINSES_R Available	1.0000	.00000	1.0000	1.0000	1.0000
RINSE5_R Busy	.12331	2.6664	.00000	1.0000	.00000
CARRIER Active	15.000	.00000	15.000	15.000	15.000
CARRIER Busy	.02566	6.1618	.00000	1.0000	.00000
POSTDIP1_R Available	1.0000	.00000	1.0000	1.0000	1.0000
POSTDIP1_R Busy	.00000		.00000	1.0000	.00000

COUNTERS

Identifier	Count	Limit
DARMO DOTTI	2616	7-61-14-
PARTS DONE	3616	Infinite

FREQUENCIES

Identifier	Category		rences AvgTime	Standard Percent	Restricted Percent
STATE (ACCELERATOR1_R)	ACCEL BATH	16	81.000	1.77	1.77
	BUSY	179	65.391	15.97	15.97
	IDLE	19 3	312.50	82.27	82.27
STATE (ACTIVATOR1_R)	BUSY	179	65.391	15.97	15.97
	IDLE	180	342.27	84.03	84.03
STATE (CLEAN1_R)	CLEAN BATH	9	66.314	0.81	0.81
	BUSY	179	65.100	15.89	15.89
	IDLE	1 8 6	328.30	83.29	83.29
STATE (ELECTROLESS1_R)	ELECT BATH	10	61.746	0.84	0.84
	BUSY	179	64.966	15.86	15.86
	IDLE	186	328.31	83.30	83.30
STATE (FLASH1_R)	FLASH BATH BUSY IDLE	6 179 184	81.000 65.491 332.09	0.66 15.99 83.35	0.66
STATE (MICROETCH1_R)	MICRO BATH	18	63.405	1.56	1.56
	BUSY	179	64.771	15.81	15.81
STATE (PREDIP1_R)	IDLE PREDIP BATH BUSY	190 8 179	318.83 64.491 65.391	82.63 0.70 15.97	82.63 0.70 15.97
STATE (TARNISH1_R)	IDLE TARN BATH	186 14	328.45 73.400	83.33 1.40	83.33 1.40
	BUSY	1 7 9	64.973	15.86	15.86
	IDLE	1 9 1	317.57	82.7 3	82.73

Execution time: 40.03 minutes. Simulation run complete.

SIMAN V - License #9999999 Systems Modeling Corporation

Summary for Replication 1 of 1

Project: TYPICAL ORGANIC PALLADIUM CONVEYORIZED Analyst: CHAD TONEY

Run execution date : 10/4/1996 Model revision date: 7/11/1996

Replication ended at time

: 45329.2

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME	.73022	7.8793	.43504	232.76	62056
TIME IN SYSTEM	28.353	.92094	14.595	119.50	62057
TIME STOPPED	81.324	.63072	.00000	226.77	221
		COUNTERS			
	Identifier		Count	Limit	
	PARTS DONE		62057	Infinite	

FREQUENCIES

Identifier	Category		rences AvgTime	Standard Percent	Restricted Percent
STATE (CLEAN_R)	CLEAN BATH	39	103.56	8.91	8.91
	BUSY IDLE	111 137	21.517 283.95	5.27 85.82	5.27 85.82
STATE (MICROETCH_R)	MICRO BATH	21	103. 6 8	4.80	4.80
	BUSY IDLE	111 126	24.406 320.97	5.98 89.22	5.98 89.22
STATE (CONDITIONER_R)	CONDI BATH	25	103.31	5.70	5.70
_	BUSY IDLE	111 130	27.955 304.94	6.85 87.46	6.85 87.46
STATE (PREDIP_R)	PREDIP BATH	21	100.53	4.66	4.66
	BUSY IDLE	111 125	29.498 319. 54	7.22 88.12	7.22 88.12
STATE (CONDUCT_R)	CONDUCT BATH	1	123.00	0.27	0.27
	BUSY IDLE	111 113	30.606 369.99	7. 4 9 92.2 3	7.49 92.23
STATE (POSTDIP_R)	POSTDIP BATH	31	111.61	7.63	7.63
	BUSY IDLE	111 133	32.685 287.52	8.00 84.36	8.00 84.36
STATE (ACID DIP_R)	ACID BATH	21	105.90	4.91	4.91
	BUSY IDLE	111 128	35.369 306.08	8.66 86.43	8.66 86.43

Execution time: 35.07 minutes. Simulation run complete.

SIMAN V - License #9999999 Systems Modeling Corporation

Summary for Replication 1 of 1

Project: TYPICAL ORGANIC PALLADIUM VERTICAL Analyst: CHAD TONEY

Run execution date : Model revision date:

9/26/1996 7/11/1996

Replication ended at time

: 31763.2

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME	8.7786	2.1695	2.0750	226.95	3615
TIME IN SYSTEM TIME STOPPED	33.349 77.536	.44838 .53042	27.575 .02500	137.57 187.45	3616 139
	DISCRI	ETE-CHANGE V	ARIABLES		
Identifier	Average	Variation	Minimum	Maximum	Final Value
CARRIER Active CARRIER Busy	13.000 .12964	.00000 2.6342	13.000	13.000 2.0000	13.600
		COUNTERS			
	Identifier		Count L	imit	
	PARTS DONE		3616 In	finite	

FREQUENCIES

Identifier	Category	Occur Number	rences AvgTime	Standard Percent	Restricted Percent
STATE (CLEAN1_R)	CLEAN BATH	23	91.783	6.65	6.65
	BUSY	77	40,221	9.75	9.75
	IDLE	94	282.50	83.60	83.60
STATE (CONDITIONER1_R)	CONDI BATH	18	89.387	5.07	5.07
	BUSY	77	41.871	10.15	10.15
	IDLE	90	299.22	84.78	84.78
STATE (PREDIP1_R)	PREDIP BATH	14	90.642	4.00	4.00
	BUSY	77	42.793	10.37	10.37
	IDLE	88	309.08	85.63	85.63
STATE (CONDUCTOR1_R)	CONDUCT BATH	2	65.158	0.41	0.41
	BUSY	77	44.891	10.88	10.88
	IDLE	79	356.66	88.71	88.71
STATE (POSTDIP1_R)	POSTDIP BATH	18	101.21	5.74	5.74
_	BUSY	77	43.271	10.49	10.49
	IDLE	90	295.65	83.77	83.77
STATE (ACID DIPL_R)	ACID BATH	22	91.494	6.34	6.34
	BUSY	77	46.718	11.33	11.33
	IDLE	95	275.29	82.34	82.34
STATE (MICROETCH1_R)	MICRO BATH	18	91.800	5.20	5.20
	BUSY	77	40.355	9.78	9.78
	IDLE	91	296.74	85.01	85.01

Execution time: 26.28 minutes. Simulation run complete.

SIMAN V - License #8810427 Systems Modeling Corporation

Summary for Replication 1 of 1

Project: CONVEYORIZED GENERIC TIN

Run execution date: Model revision date: 6/10/1997

Analyst: CHAD TONEY

7/11/1996

Replication ended at time

: 26082.6

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME	.42017	11.661	. 27134	190.00	62056
TIME IN SYSTEM TIME STOPPED	64.169 93.815	1.1194 .90075	8.6078 10.000	433.99 241.52	62057 96
	DISCRI	ETE-CHANGE V	ARIABLES		
Identifier	Average	Variation	Minimum	Maximum	Final Value
# in TO_CLEANER_Q	.03874	4.9813	.00000	1.0000	.00000
		COUNTERS			
	Identifier		Count	Limit	
	PARTS DONE		62057	Infinite	

FREQUENCIES

Identifier	Category	Occur Number	rences AvgTime	Standard Percent	Restricted Percent
STATE (CLEAN_R)	CLEAN BATH	9	181.61	6.27	6.27
	BUSY	63	4.9883	1.20	1.20
	IDLE	71	339.91	92.53	92.53
STATE (MICROETCH R)	MICRO BATH	21	129.85	10.45	10.45
	BUSY	63	23.525	5.68	5.68
	IDLE	76	287.81	83.86	83.86
STATE (PREDIP R)	PREDIP BATH	15	149.46	8.60	8.60
	BUSY	63	32.337	7.81	7.81
	IDLE	72	302.82	83.59	83.59
STATE (ACID DIP R)	ACID BATH	7	122.88	3.30	3.30
	BUSY	63	42.546	10.28	10.28
	IDLE	64	352.21	86.43	86.43
STATE (CATALYST R)	BUSY	63	32.337	7.81	7.81
	IDLE	64	375.70	92.19	92.19
STATE (ACCELERATOR R)	ACCEL BATH	7	153.10	4.11	4.11
· _ ·	BUSY	63	35.931	8.68	8.68
	IDLE	68	334.51	87.21	87.21
	IDUG	00	224.31	07.21	01.21

Execution time: 23.80 minutes.

Simulation run complete.

SIMAN V - License #8810427 Systems Modeling Corporation

Summary for Replication 1 of 1

Project: VERTICAL GENERIC TIN STA

Analyst: CHAD TONEY

Run execution date : Model revision date:

6/10/1997 7/11/1996

Replication ended at time

: 48525.4

TALLY VARIABLES

Identifier	Average	Variation	Minimum	Maximum	Observations
TAKT TIME	13.409	1.9911	9.2750	294.97	3615
TIME IN SYSTEM	52.839	.08080	50.000	65.625	3616
TIME STOPPED	102.49	.73478	.00000	286.32	133
	DISCRI	ETE-CHANGE V	ARIABLES		
Identifier	Average	Variation	Minimum	Maximum	Final Value
CARRIER Active	11.000 .06573	.00000 3.8295	11.000 .00000	11.000 2.0000	11.000
		COUNTERS			
	Identifier		Count 1	Limit	
	PARTS DONE		3616 I	nfinite	

FREQUENCIES

Identifier	Category		rences AvgTime	Standard Percent	Restricted
				· · · · · · · · · · · · · · · · · · ·	
STATE (CLEAN1_R)	CLEAN BATH	7	170.93	2.47	2.47
	BUSY	119	63.565	15.59	15.59
	IDLE	121	328.63	81.95	81.95
STATE (MICROETCH1 R)	MICRO BATH	18	202.66	7.52	7.52
_	BUSY	119	63.707	15.62	15.62
	IDLE	127	293.67	76.86	76.86
STATE (PREDIP1_R)	PREDIP BATH	10	67.055	1.38	1.38
_	BUSY	119	75.149	18.43	18.43
	IDLE	120	324.26	80.19	80.19
STATE (CATALYST1_R)	BUSY	119	75.149	18.43	18.43
_	IDLE	119	332.62	81.57	81.57
STATE (ACCELERATOR1 R)	ACCEL BATH	7	107.83	1.56	1.56
- ·	BUSY	119	74.082	18.17	18.17
	IDLE	125	311.63	80.28	80.28
STATE (ACID DIP1_R)	ACID BATH	8	159.12	2.62	2.62
	BUSY	119	77.569	19.02	19.02
	IDLE	121	314.22	78.35	78.35

Execution time: 36.25 minutes. Simulation run complete.

G.5	Chemical Costs by Bath for Individual MHC Processes
	Total Materials Cost by MHC Alternative

Process: Electroless Copper Supplier #1

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	75.3	A	6	\$25.45/gal	\$98.79	\$114.98
Microetch	64.3	75.3	В	13.8 g/l	\$2.57/lb	\$50.27	\$58.87
			С	2.5	7.62/gal		
			D	18.5	\$1.60/gal		
Predip	49.8	75.3	Е	31.725 g/l	\$1.31/lb	\$14.65	\$22.15
			F	1.5	\$2.00/gal		
Catalyst	138.5	75.3	G	4	\$391.80/gal	\$2,180.53	\$1,185.52
			Н	0.176 g/l	\$1.31/lb		
			I	3.5	\$2.00/gal		
Accelerator	79.5	75.3	J	20	\$18.10/gal	\$287.79	\$272.59
Electroless Copper	185	75.3	K	7	\$27.60/gal	\$617.92	\$251.51
			L	8.5	\$16.45/gal		
			M	0.22	\$4.50/gal		
Neutralizer	57	75.3	N	100	\$1.60/gal	\$91.20	\$120.48
Anti-Tarnish	38.6	75.3	О	0.25	\$39.00/gal	\$3.76	\$7.33

Process: Electroless Copper Supplier #2

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	75.3	A	6	\$25.45/gal	\$98.79	\$114.98
Microetch	64.3	75.3	В	13.8 g/l	\$2.57/lb	\$50.27	\$58.87
			C	2.5	7.62/gal		
			D	18.5	\$1.60/gal		
Predip	49.8	75.3	Е	31.725 g/l	\$1.31/lb	\$14.65	\$22.15
			F	1.5	\$2.00/gal		
Catalyst	138.5	75.3	G	4	\$391.80/gal	\$2,180.53	\$1,185.52
			Н	0.176 g/l	\$1.31/lb		
			I	3.5	\$2.00/gal		
Accelerator	79.5	75.3	J	20	\$18.10/gal	\$287.79	\$272.59
Electroless Copper	185	75.3	K	2.75	\$27.60/gal	\$623.45	\$253.76
		Ì	L	1.75	\$12.90/gal	1	
			M	14.5	\$16.45/gal		
Neutralizer	57	75.3	N	100	\$1.60/gal	\$91.20	\$120.48
Anti-Tarnish	38.6	75.3	0	0.25	\$39.00/gal	\$3.76	\$7.33

Process: Electroless Copper Supplier #3

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	75.3	A	10	\$36.68/gal	\$356.00	\$414.32
			В	5	\$28.78/gal		
			C	2.5	\$15.81/gal		
Microetch	64.3	75.3	D	9.8 g/l	\$2.62/lb	\$16.32	\$19.11
			Е	2.5	\$1.60/gal		
Predip	49.8	75.3	F	75	\$5.39/gal	\$201.32	\$304.41
Activator/Palladium	57	75.3	G	1	\$497.71/gal	\$514.12	\$679.18
			Н	75	\$5.39/gal		
Accelerator	79.5	75.3	I	8.96 g/l	\$497.71/lb	\$3,013.94	\$2,854.71
			J	1	\$77.71/gal		
Electroless Copper	185	75.3	K	4	\$11.51/gal	\$433.14	\$176.30
			L	10	\$15.44		
			M	0.2	\$19.36/gal		
			N	3	\$9.19/gal		
			О	0.5	\$4.50/gal		
Anti-Tarnish	38.6	75.3	P	1	\$28.26/gal	\$10.90	\$21.26

Process: Electroless Copper Supplier #4

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	75.3	A	12.5	\$10.30/gal	\$83.30	\$96.95
Microetch	64.3	75.3	В	5	\$12.32/gal	\$84.68	\$95.65
			C	3	\$13.81/gal		
			D	15	\$1.60/gal		
Predip	49.8	75.3	Е	75	\$2.79/gal	\$104.21	\$157.57
Activator/Palladium	57	75.3	F	3.8	\$211.35/gal	\$638.35	\$843.29
			G	1	\$128.59/gal		
			Н	579.5 g/l	\$0.39/lb		
Accelerator	79.5	75.3	I	5	\$16.47/gal	\$144.65	\$137.01
			J	15	\$6.64/gal		
Electroless Copper	185	75.3	K	5	\$9.57/gal	\$393.16	\$160.03
			L	1.5	\$9.22/gal		
			M	12	\$12.57/gal		
Acid Dip	78.8	75.3	N				
Anti-Tarnish	38.6	75.3	0	0.25	\$14.07	\$1.36	\$2.65

Process: Electroless Copper Supplier #5

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	75.3	A	15	\$26.50/gal	\$257.18	\$299.31
Microetch	64.3	75.3	В	60 g/l	\$2.57/lb	\$83.59	\$97.89
			С	1	\$1.60/gal		
Predip	49.8	75.3	D	1165 g/l	\$1.59/gal	\$768.14	\$1,161.46
Palladium Catalyst	138.5	75.3	Е	3	\$497/gal	\$2,280.00	\$1,239.60
			F	97	\$1.59/lb		
Electroless Copper	185	75.3	G	4.2	\$19.29/gal	\$1,834.31	\$746.61
			Н	10	\$29.37/gal		
			I	12	\$51.40/gal		
Anti-Tarnish	38.6	75.3	J	2.5	\$20.50/gal	\$21.63	\$42.20
		· ·	K	3	\$1.60/gal]	

Process: Electroless Copper

Supplier #6

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	75.3	A	0.5	\$22.70/gal	\$77.87	\$90.63
			В	4	\$26.88/gal		
			С	2.5	\$0.594/g		
Predip	49.8	75.3	D	5	\$99.29/gal	\$247.22	\$373.81
Activator	57	75.3	Е	25	\$147.5/gal	\$2,101.89	\$2,776.71
			F	0.5	\$0.0594/g	1	
Reducer	57	75.3	G	0.5	\$147.5/gal	\$42.03	\$55.52
			Н	5 g/l	\$.795/lb		
Electroless Copper	185	75.3	I	1.4	No data		
			J	8	No data	1	
			K	0.15	No data		
		,	L	3	No data	1	

Process: Formaldehyde-Free Electroless Copper Supplier #1

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	No data	75.3	A	10	\$36.68/gal	No data	\$384.56
			В	5	\$28.78/gal		
Microetch	No data	75.3	С	9.8 g/l	\$2.62/lb	No data	\$19.11
			D	2.5	\$1.60/gal		
Predip	No data	75.3	Е	75	\$6.38/gal	No data	\$360.31
Activator	No data	75.3	F	1.5	\$497.71/gal	No data	\$562.17
			G	75	\$6.38/gal		
Accelerator	No data	75.3	Н	8.96 g/l	\$497.71/gal	No data	\$2,854.70
			I	1	\$77.71/gal		
Electroless Copper	No data	75.3	J	11	\$92.96/gal	No data	\$1,633.84
			K	5.5	\$14.18/gal		
			L	32	\$24.99/gal		
			M	25 g/l	\$5.49/lb	1	
		,	N	15 g/l	\$12.43/lb		
Anti-Tarnish	No data	75.3	О	1	\$28.61/gal	No data	\$21.54

Process: Organic-Palladium Supplier #1

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner	44	75.3	A	5	\$36.38/gal	\$104.95	\$180.45
			В	5	\$11.55/gal		
Microetch	64.3	75.3	С	75 g/l	\$16.20/gal	\$650.54	\$761.83
Predip	49.8	75.3	D	100	No data	No data	No data
Conductor	108	75.3	Е	10	\$36.38/gal	\$534.6	\$372.74
			F	10	\$13.12/gal		
Post-Dip	45	75.3	G	20	\$17.42/gal	\$156.78	\$262.35
Acid Dip Bath	78.8	75.3	Н	No data	No data	No data	No data
Conditioner	56	75.3	I	5	\$36.38/gal	\$133.58	\$180.45
			J	5	\$11.55/gal		

Process: Tin-Palladium

Supplier #1

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	75.3	A	25	\$22.90/gal	\$370.41	\$431.10
Microetch	64.3	75.3	В	149.8 g/l	\$3/lb	\$241.14	\$282.39
			С	0.5	\$1.60/gal		
Predip	49.8	75.3	D	100	\$12.75/gal	\$634.95	\$960.08
Activator	138.5	75.3	Е	95	\$12.75/gal	\$6,871.33	\$3,735.82
			F	5	\$750/gal		
Accelerator	79.5	75.3	G	25	\$13.20/gal	\$724.44	\$686.17
			Н	25	\$23.25/gal		
Acid Dip Bath	78.8	75.3	I	10	\$1.60/gal	\$12.61	\$12.05

Process: Tin-Palladium

Supplier #2

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Conditioner	55.7	75.3	A	15	\$31.38/gal	\$292.13	\$394.93
			В	2.5	\$21.58/gal		
Predip	49.8	75.3	С	100	\$5.94/gal	\$295.18	\$447.28
Palladium Catalyst	138.5	75.3	D	92	\$5.94/gal	\$5,411.36	\$2,942.06
			Е	8	\$420.80/gal		
Accelerator	79.5	75.3	F	20	\$68.75/gal	\$1,093.12	\$1,035.37
Enhancer	57	75.3	G	2	\$5.14/gal	\$25.81	\$34.10
			Н	2	\$17.50/gal		
Stabilizer	57	75.3	I	2	\$17.50/gal	\$19.95	\$26.36
Microetch	64.3		J	7	\$25.79/gal	\$318.13	\$372.55
			K	2.5	\$104.29/gal		
			L	10	\$1.60/gal		
			M	5	\$7.50/gal		

Process: Tin-Palladium

Supplier #3

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Conditioner	55.7	75.3	A	1	\$83.30/gal	\$46.40	\$62.73
Microetch	64.3	75.3	В	175 g/l	\$1.50/lb	\$140.55	\$164.59
Predip	49.8	75.3	С	100	\$2.95/gal	\$209.35	\$316.55
Catalyst	138.5	75.3	D	95	\$5.95/gal	\$6,634	\$3,607.00
			Е	5	\$845/gal		
Accelerator	79.5	75.3	F	0.045 g/l	No data	No data	No data
			G	1.2			
Acid Stabilizer	78.8	75.3	Н	10	\$1.60/gal	\$12.61	\$12.05

Process: Carbon Supplier #1

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner	44	No data	A	5	\$90.43/gal	\$198.94	No data
Conditioner	55.7	No data	В	2.5	\$192.17/lb	\$267.60	No data
Carbon Black	128	No data	С	100	\$153.98/gal	\$19,709.44	No data
Microetch	64.3	No data	D	200 g/l	\$1.17/lb	\$126.03	No data
			Е	1	\$1.60/gal		

Process: Graphite Supplier #1

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Cleaner/Conditioner	64.7	No data	A	25	\$47.83/gal	\$773.66	No data
Graphite	36.5	No data	В	60	\$675/gal	\$14,782.50	No data
Fixer	57	No data	С	10	\$16.50/gal	\$94.05	No data
Microetch	64.3	No data	D	55	\$9.32/gal	\$331.66	No data
			Е	2	\$1.60/gal		

Process: Conductive Polymer Supplier #1

Bath	Volume in Bath (in gallons) Horizontal	Volume in Bath (in gallons) Vertical	Chemical Name	Percentage of Chemical in Bath	Cost of Chemicals	Total Cost of the Bath (Horizontal)	Total Cost of the Bath (Vertical)
Microetch	64.3	No data	A	2	\$1.60/gal	\$27.64	No data
		No data	В	7.5 Kg	\$3.41/Kg		No data
Cleaner/Conditioner	64.7	No data	С	10	\$21.90/gal	\$140.82	No data
Catalyst	138.5	No data	D	81.5	\$36.90/gal	\$4,183.90	No data
		No data	Е	0.3	\$4.00/gal		No data
		No data	F	0.5	\$24.60/gal		No data
Conductive Polymer	26	No data	G	15	\$90.30/gal	\$460.70	No data
		No data	Н	23	\$17.40/gal		No data
		No data	I	0.7	\$24.60/gal		No data

Summary average cost per bath

Process: Electroless Copper

Bath	Total Bath	Replacement	Annual	Total Bath	Replacement	Annual
	Cost	Frequency	Cost	Cost	Frequency	Cost
	(Conveyorized)	(Conveyorized)	(Conveyorized)	(Non-	(Non-	(Non-
				Conveyorized)	Conveyorized)	Conveyorized)
Cleaner/ Conditioner	\$161.99	10	\$1,619.90	\$188.53	9	\$1,696.77
Microetch	\$57.03	21	\$1,197.63	\$66.08	18	\$1,189.44
Predip	\$225.03	13	\$2,925.39	\$340.26	8	\$2,722.08
Catalyst	\$1,649.24	1	\$1,649.24	\$1,318.30	1	\$1,318.30
Accelerator	\$755.24	15	\$11,328.60	\$718.48	16	\$11,495.68
Electroless Copper	\$779.29	4	\$3,117.16	\$317.19	10	\$3,171.90
Neutralizer	\$91.20	6	\$547.20	\$120.48	6	\$722.88
Anti-Tarnish	\$9.41	28	\$263.48	\$16.15	13	\$209.95
Total			\$22,648.60			\$22,527.00

Process: Formaldehyde-Free Electroless Copper

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Bath	Total Bath	Replacement	Annual	Total Bath	Replacement	Annual
	Cost	Frequency	Cost	Cost	Frequency	Cost
	(Conveyorized)	(Conveyorized)	(Conveyorized)	(Non-	(Non-	(Non-
				Conveyorized)	Conveyorized)	Conveyorized)
Cleaner/						
Conditioner	NA	NA	NA	\$384.56	9	\$3,461.04
Microetch	NA	NA	NA	\$19.11	18	\$343.98
Predip	NA	NA	NA	\$360.31	8	\$2,882.48
Activator	NA	NA	NA	\$562.17	1	\$562.17
Accelerator	NA	NA	NA	\$2,854.70	16	\$45,675.20
Electroless						
Copper	NA	NA	NA	\$1,633.84	10	\$16,338.40
Anti-Tarnish	NA	NA	NA	\$21.54	14	\$301.56
Total						\$69,564.83

Process: Organic Palladium

Bath	Total Bath	Replacement	Annual	Total Bath	Replacement	Annual
	Cost	Frequency	Cost	Cost	Frequency	Cost
	(Conveyorized)	(Conveyorized)	(Conveyorized)	(Non-	(Non-	(Non-
				Conveyorized	Conveyorized	Conveyorized
)))
Cleaner	\$155.05	39	\$6,046.95	\$180.45	23	\$4,150.35
Microetch	\$650.54	21	\$13,661.34	\$761.83	18	\$13,714.74
Conditioner	\$133.58	25	\$3,339.50	\$180.45	18	\$3,248.10
Predip	-	21	-	-	14	-
Conductor	\$534.60	1	\$534.60	\$372.74	2	\$745.48
Post Dip	\$156.78	31	\$4,860.18	\$262.35	18	\$4,722.30
Acid Dip						
Bath	\$19.95	21	\$418.95	\$19.02	22	\$418.34
Total			\$28,861.52			\$26,999.31

^{*}Acid Dip assumed to be similar in price to acid dip for tin palladium.

Process: Tin-Palladium

Bath	Total Bath Cost	Replacement Frequency	Annual Cost	Total Bath Cost	Replacement Frequency	Annual Cost
			(Conveyorized)		(Non-	(Non-
					Conveyorized)	,
Cleaner/ Conditioner	\$236.31	9	\$2,126.79	\$296.25	7	\$2,073.75
Microetch	\$233.27	21	\$4,898.67	\$273.18	18	\$4,917.24
Predip	\$380.04	15	\$5,700.60	\$574.61	10	\$5,746.10
Catalyst	\$6,305.56	1	\$6,305.56	\$3,428.29	1	\$3,428.29
Accelerator	\$908.78	7	\$6,361.46	\$860.77	7	\$6,025.39
Acid Dip Bath	\$15.06	7	\$105.42	\$16.82	8	\$134.56
Total			\$25,498.50			\$22,325.33

^{*} Some processes included an enhancer bath that will not be included in analysis.

Process: Carbon

Bath	Total Bath Cost	Replacement Frequency	Annual Cost	Total Bath Cost	Replacement Frequency	Annual Cost
	(Conveyorized)	(Conveyorized)	(Conveyorized)	(Non-	(Non-	(Non-
				Conveyorized)	Conveyorized)	Conveyorized)
Cleaner	\$198.94	26	\$5,172.44	NA	NA	NA
Conditioner	\$267.60	20	\$5,352.00	NA	NA	NA
Carbon Black ¹	\$19,709.44	1	\$19,709.44	NA	NA	NA
Microetch	\$126.03	21	\$2,646.63	NA	NA	NA
Total			\$32,880.51	NA	NA	NA

¹ Carbon had no bath replacements in the simulation, however, at least one bath out of two would more than likely have been replaced.

Process: Graphite

Bath	Total Bath	Replacement	Annual	Total Bath	Replacement	Annual
	Cost	Frequency	Cost	Cost	Frequency	Cost
	(Conveyorized)	(Conveyorized)	(Conveyorized)	(Non-	(Non-	(Non-
				Conveyorized	Conveyorized	Conveyorized
)))
Cleaner/						
Conditioner	\$773.66	11	\$8,510.26	NA	NA	NA
Graphite	\$14,782.50	3	\$44,347.50	NA	NA	NA
Fixer	\$94.05	NA	NA	NA	NA	NA
Microetch	\$331.66	21	\$6,964.86	NA	NA	NA
Total			\$59,822.62	NA	NA	NA

Process: Conductive Polymer¹

Bath	Total Bath Coat	Replacement Frequency	Annual Cost	Total Bath Cost	Replacement Frequency	Annual Cost
	(Conveyorized)				(Non-	(Non-
		(3011, 6) 311164)	• •	Conveyorized	(· · -	(· · -
)))
Microetch		21		Not Avail.	NA	NA
Cleaner/						
Conditioner		13		Not Avail.	NA	NA
Catalyst		1		Not Avail.	NA	NA
Conductive Polymer		6		Not Avail.	NA	NA
Total						

¹ Cost data were not available for all chemical products when this analysis was completed. These costs will be included in the final analysis.

G.6 Sensitivity Analyses

